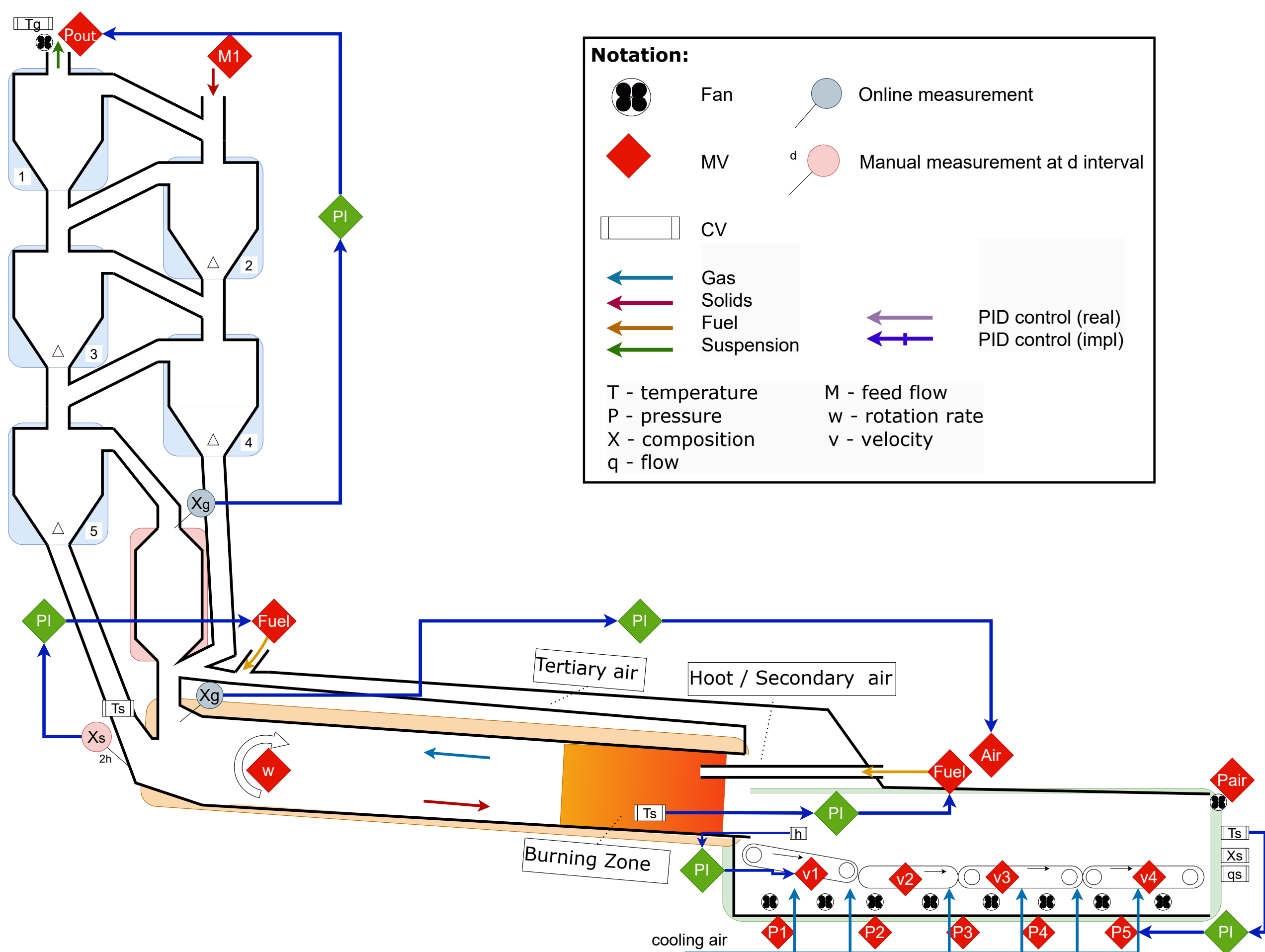
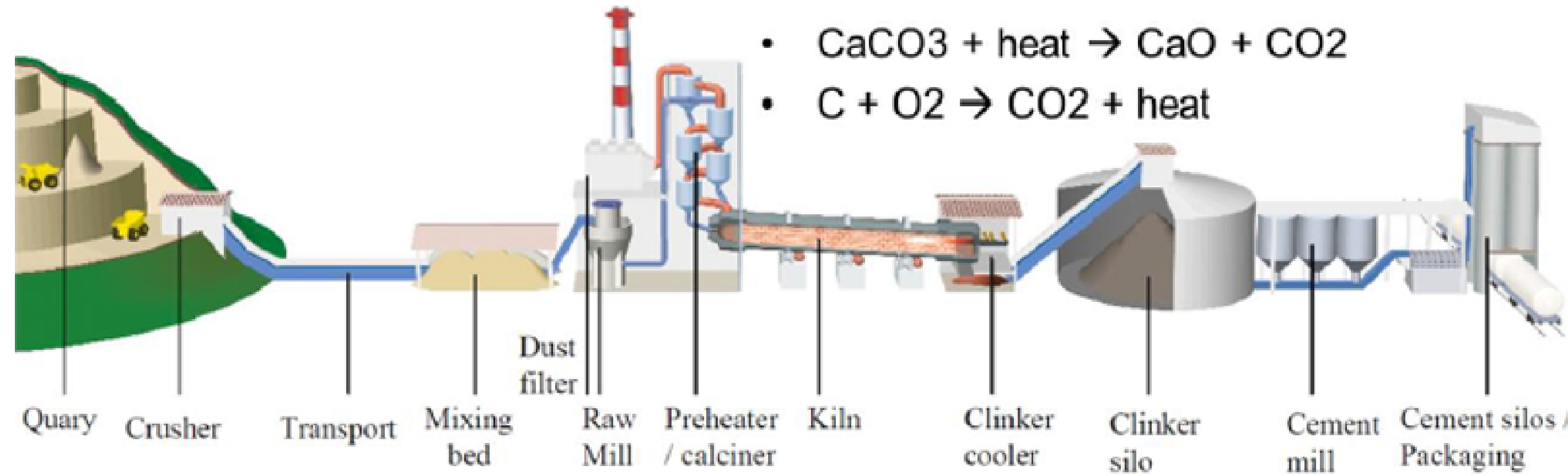


Model-Based Control for the Cement Industry

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1. Cement manufacturing and the pyro-section



2. DAE of the pyro-section

DAE structure

$$\begin{aligned} \dot{x} &= f(x, y, u) \\ 0 &= g(x, y, u) \\ z &= h(x, y, u) \end{aligned}$$

Mass and energy balances

$$\begin{aligned} \partial_t c &= -\nabla \cdot N + R \\ \partial_t \hat{U} &= -\nabla \cdot \tilde{H} + Q \end{aligned}$$

Algebraic relations

$$\begin{aligned} U(T, P, c) - \hat{U} &= 0 \\ V(T, P, c) - 1 &= 0 \end{aligned}$$

Thermo-physical properties

$$\begin{aligned} V &= V(T, P, n) \\ H &= H(T, P, n) \\ U &= H(T, P, n) - PV(T, P, n) \\ C_p &= C_p(T, n) \\ \rho &= M'c \\ \mu &= \mu(T, n, \hat{V}) \\ k &= k(T, n, \hat{V}) \\ D &= D(T, P, c) \end{aligned}$$

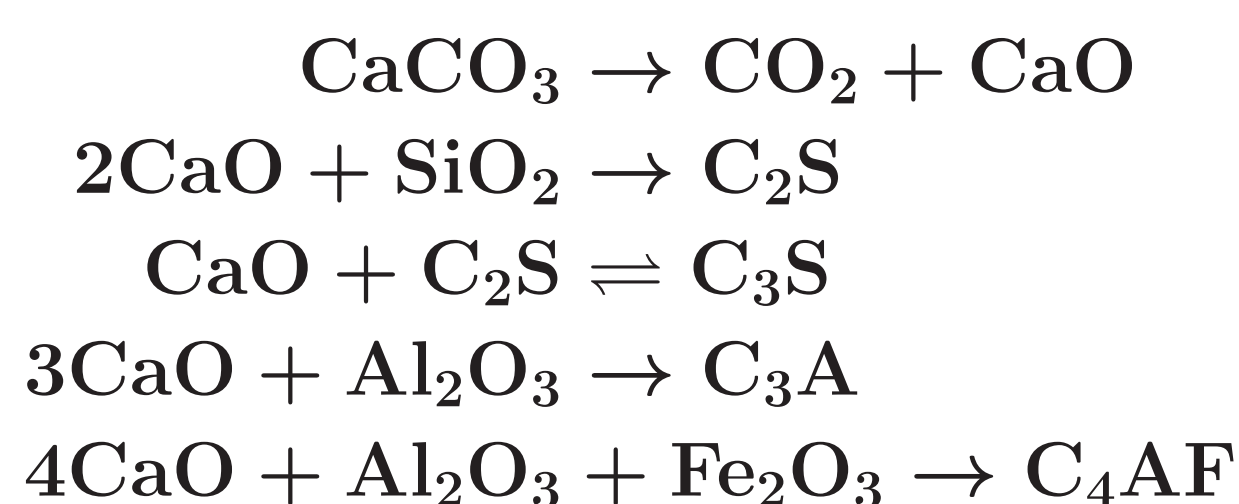
Transport phenomena

$$\begin{aligned} N &= cv - D\nabla c \\ \tilde{H} &= H(T, P, N) - k\nabla T \\ v &= v(\nabla P, \mu, \rho) \\ Q &= Q(T, P, n, k, \mu, \rho, C_p) \end{aligned}$$

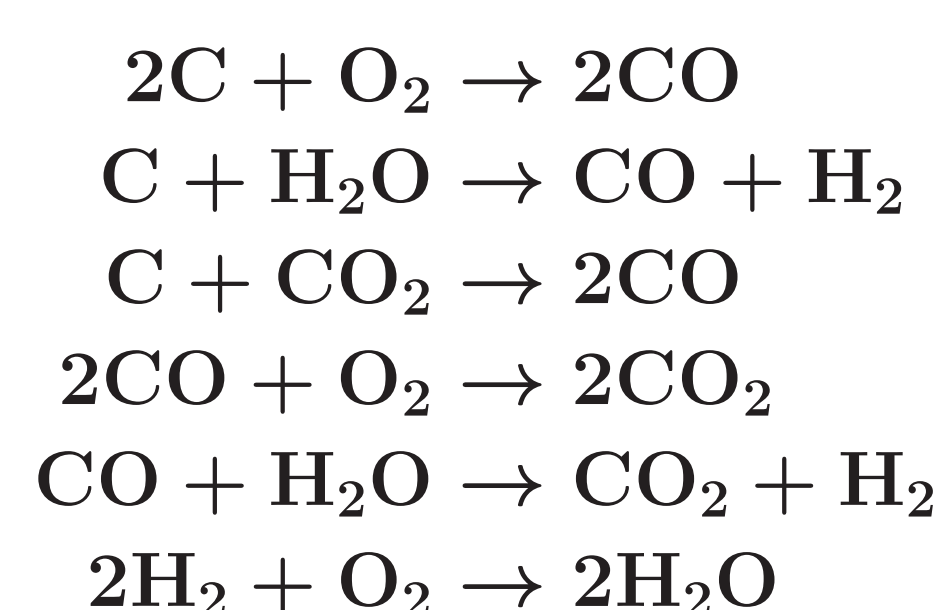
Reaction and production rates

$$R = \nu' r(T, P, c)$$

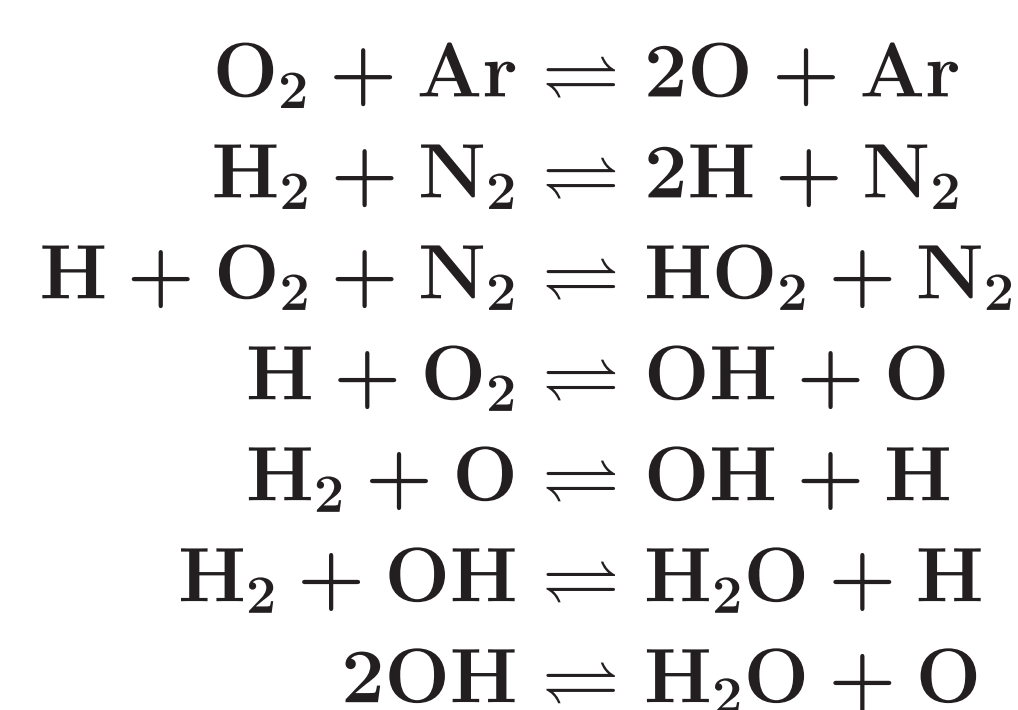
Clinker formation reactions



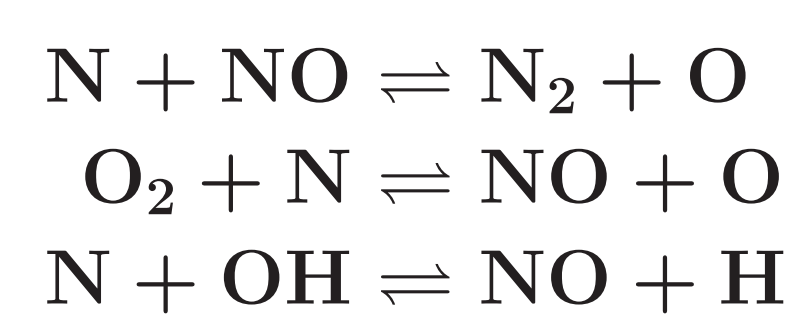
Combustion reactions



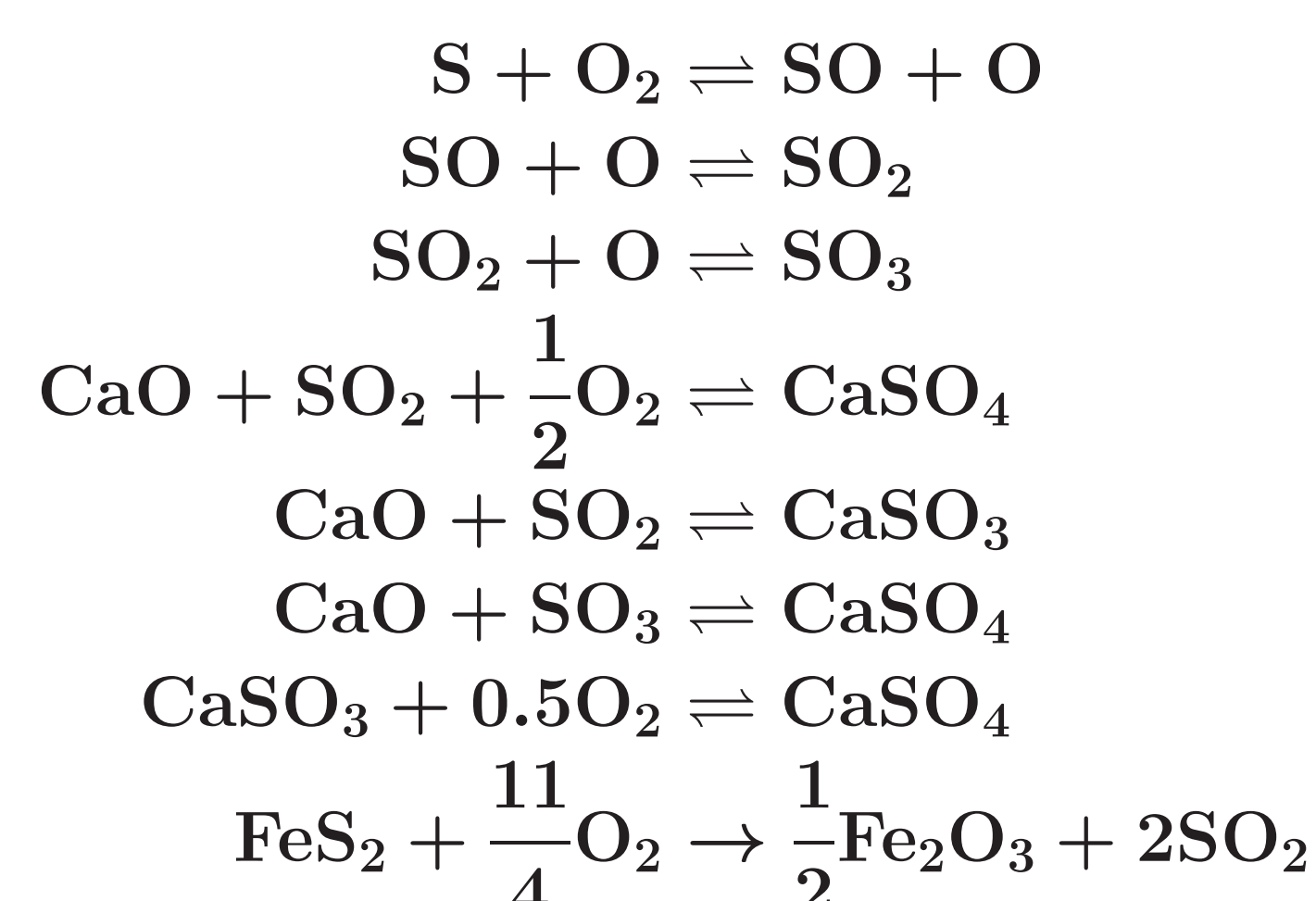
Radical reactions



NOx reactions

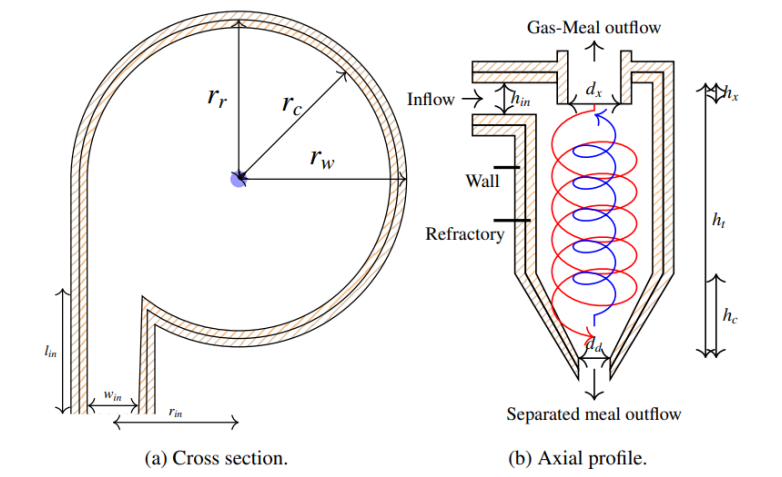


SOx reactions



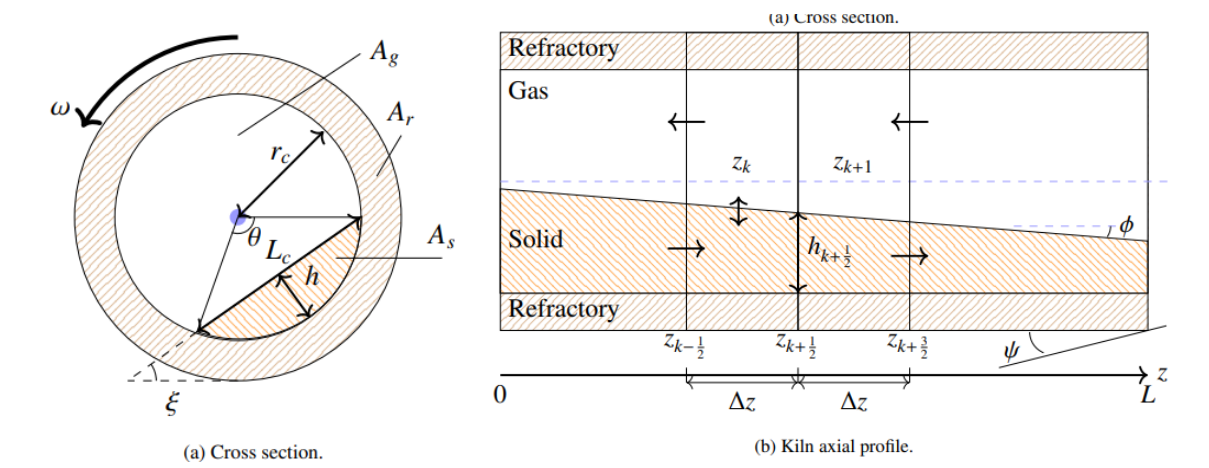
Cyclone specific model formulas

$$v_{sep} = \frac{d_m^2 \Delta \rho v_{\theta, req} (v_{in})^2}{18 \mu_m r_{eq}}, \quad r_{eq} = \sqrt{\frac{V_{\Delta}}{\pi h_t}}$$



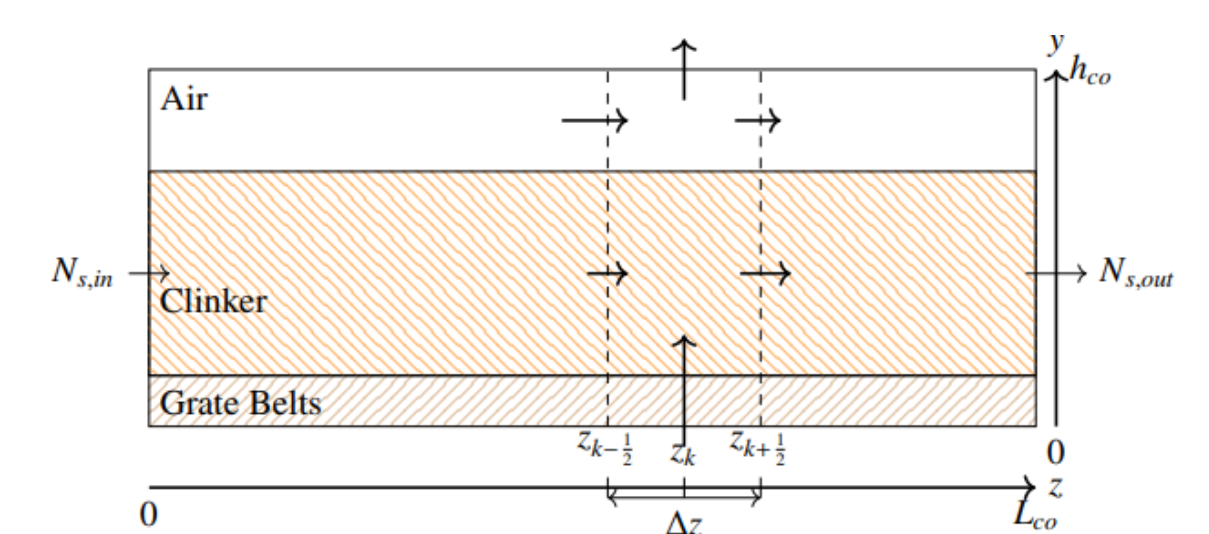
Kiln specific model formula

$$v_s(z) = \omega \frac{\psi + \phi(z) \cos(\xi)}{\sin(\xi)} \frac{\pi L_c(z)}{\text{asin}(\frac{L_c(z)}{2r_c})}$$



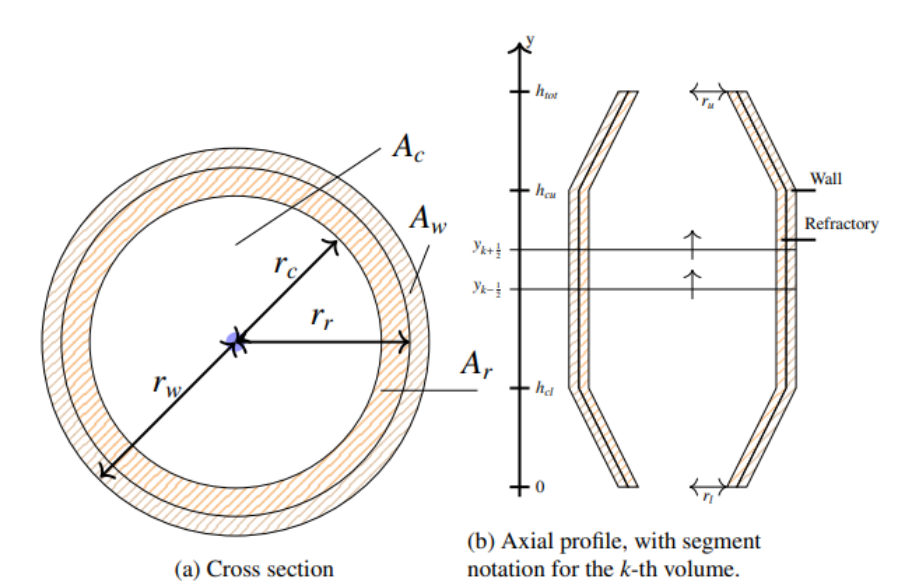
Cooler specific model formulas

$$\begin{aligned} Q_{ij}^{cv} &= A_{ij} \beta_{ij} (T_i - T_j) \\ \beta &= \frac{k_s Nu}{D_p + 0.5 \phi D_p Nu} \\ Nu &= 2 + 1.8 Pr^{\frac{1}{3}} Re^{\frac{1}{2}} \end{aligned}$$



Calcliner specific model formulas

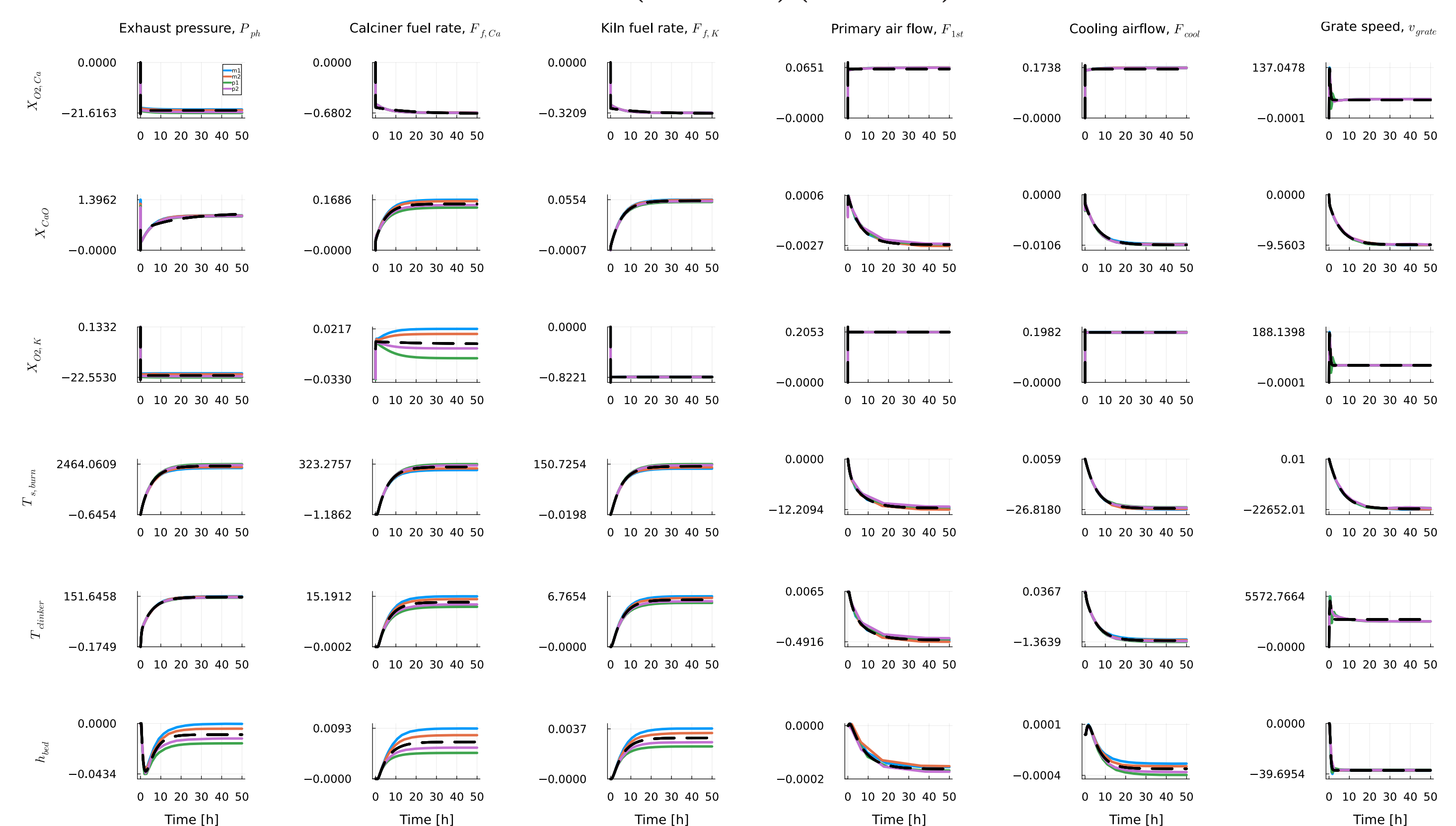
$$\begin{aligned} \beta_m &= \frac{k_m}{D_H} Nu \\ Nu &= \frac{\frac{f}{8}(Re_D - 1000) Pr}{1 + 12.7(\frac{f}{8})^{\frac{1}{2}}(Pr^{\frac{2}{3}} - 1)} \end{aligned}$$



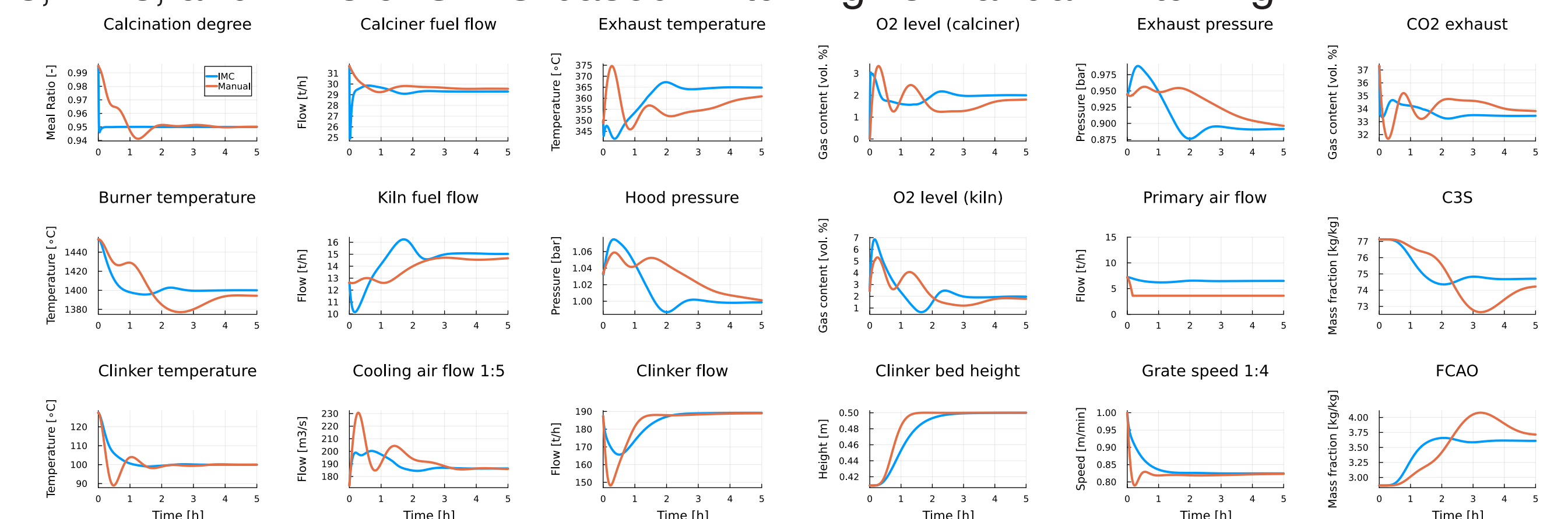
3. Model-based step response & IMC-based tuning

Normalized step response from the model and the estimated linear transfer function

$$\hat{g}(s) = K_0 \frac{\tau_z s + 1}{(\tau_1 s + 1)(\tau_2 s + 1)} e^{-\tau_d s}$$



CVs, MVs, and KPIs of SIMC-based PI-tuning vs manual PI-tuning



4. RGA

Linearized system

$$\begin{aligned} G(s) &= C(sI - A)^{-1}B + D \\ A &= \partial_x f - \partial_y f [\partial_y g]^{-1} \partial_x g \\ B &= \partial_u f - \partial_y f [\partial_y g]^{-1} \partial_u g \\ C &= \partial_x h - \partial_y h [\partial_y g]^{-1} \partial_x g \\ D &= \partial_u h - \partial_y h [\partial_y g]^{-1} \partial_u g \end{aligned}$$

CV-MV pairing evaluation based on RGA

$$\Lambda_{\omega}(G) = G(i\omega) \circ (G(i\omega)^{-1})^T$$

$$[\Phi_{\omega}]_{ij} = \frac{1}{[\Lambda_{\omega}(G)]_{ij}} - 1$$

Table 1: RGA matrix.

Intuitive pairs (blue,orange).
RGA-based pairs (red,orange).

CV\MV	v_{grate}	P_{ph}	F_{feed}	$F_{f, Ca}$	$F_{f, K}$	F_{1st}	F_{cool}
$X_{O_2, Ca}$	-7e-6	5.20	-0.08	-1.13	1.61	-2.17	-2.43
X_{CaO}	1e-5	-6.62	1.30	13.4	-14.4	3.87	3.51
$X_{O_2, K}$	8e-5	-3.56	-0.02	-0.01	-4.23	7.14	1.69
$T_{s, burn}$	-0.01	8.54	-1.38	-11.7	19.4	-8.35	-5.51
F_{clink}	1e-3	-0.17	1.04	2e-3	0.01	0.04	0.08
$T_{clinker}$	-2e-6	-2.41	0.18	0.42	-1.26	0.45	3.61
h_{bed}	1.01	0.02	-0.04	0.02	-0.08	0.02	0.05